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(54) Title: CLAY ACTIVATION WITH METAL SALTS (57) Abstract High performance activated clays suitable for bleaching oil are produced by mixing a clay mineral with a metal salt that is a Lewis acid. Mixtures of such metal salts can be used as well.		

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CLAY ACTIVATION WITH METAL SALTSTechnical Field

5 This invention relates to clay-based compositions suitable for the bleaching of oil. In particular, the present invention is directed to oil bleaching compositions treated with a multivalent metal salt that is a Lewis acid.

Background of the Invention

10 Fats and fatty oils, commonly called triglycerides, are constituted of triesters of glycerol, and include minor amounts of fatty acids. At ambient temperatures, about 20 degrees C to about 25 degrees C, fats are solids, whereas fatty oils are liquids.

15 Triglycerides are widely distributed in nature. Some triglycerides are edible while others are not. Many are derived directly from vegetable, animal, and marine sources. Others are obtained, as by-products, in the production of fiber from vegetable matter, and in the production of protein from vegetable, animal or marine matter.

20 Edible vegetable oils include canola, coconut, corn germ, cottonseed, olive, palm, peanut, rapeseed, safflower, sesame seed, soybean, and sunflower oils. Examples of nonedible vegetable oils are jojoba oil, linseed oil and castor oil.

25 Illustrative sources of edible animal-derived oil include lard and tallow. Examples of nonedible animal-derived oil are low grade tallow and neat's-foot oils.

30 Some of these oils may have a color that is objectionable to a consumer. Thus, the oil needs to be bleached to improve its color quality. To this end, a great many oils are commonly treated with bleaching clays to reduce oil color values by adsorptive

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purification. Bleaching clays generally improve oil color quality by adsorbing color impurities that are present. Color impurities typically present in oils include, for example, carotenoids, xanthophylls, xanthophyll esters, chlorophyll, tocopherols, as well as oxidized fatty acids and fatty acid polymers.

It is also desirable to remove color impurities from a nonedible oil to obtain a acceptable color.

Natural clays, e.g., Fuller's earth and the bentonites, have commonly been used as bleaching clays to remove both the naturally-occurring and the otherwise-present, e.g., the thermally-induced, color impurities from edible and nonedible oils. It has been suggested that clays containing a zeolite can be used for such a purpose as well.

Acid-activated clays have also been used for this purpose. Such clays generally remove a relatively wider spectrum of color impurities.

However, addition of an inorganic acid, such as sulfuric acid, to clay has an adverse effect on the clay lattice. The acid tends to cause degradation of the lattice with attendant product stability problems.

Shelf life also can be a major problem with all commercially available bleaching clays. Significant degradation in product bleaching activity may occur initially after manufacturing. Degradation rate declines with time, but still continues.

A conventional process for producing acid-activated bleaching clays utilizes calcium bentonite clays and sulfuric acid. The calcium bentonites used in the acid activation process typically are neutral to mildly basic. The acidic salts formed during activation and residual acid can be washed off

and separated by filtration from the product clay, if desired. However it is not necessary to do so.

Another type of naturally-occurring clay, frequently classified as palygorskite clays, requires heat to impart bleaching activity. Mineralogically, the palygorskite clays are distinguishable from the bentonites (smectites, including montmorillonites).

Summary of the Invention

Highly active clay-derived bleaching compositions are obtained by the activation of a clay mineral by metal salts that are Lewis acids. Activation in this manner can be effected at ambient temperatures, and in a relatively short time period of the order of minutes. After activation, the obtained product is air dried, size reduced and classified if desired, and is then ready for use.

Surface acidity, along with surface area, pore size distribution and pore volume, is an important clay characteristic affecting the ability of a clay to remove chlorophyll from oils. Cations of aluminum, iron and titanium, which coat the surface of the some clays, are major factors that enhance the clays' ability to remove pigments such as chlorophyll from oils. The addition of such Lewis acid metal salts to the raw clay enhances the clay's ability to remove pigments from oils and improves the stability of the enhanced clay.

Brief Description of the Drawings

In the drawings,
FIGURE 1 shows the distribution of pore volumes within pore size classes produced by treatment with Lewis acid metal salts compared to treatment with sulfuric acid;

FIGURE 2 shows bleaching isotherms comparing the clay composition of the present invention and two commercially available bleaching clays; and

5 FIGURE 3 shows the results of a study in which the stability of the clay composition of the present invention and two commercially available bleaching clays were compared.

Description of the Embodiments

10 While this invention is susceptible to embodiments in many different forms, preferred embodiments of the invention are described below. It should be understood, however, that the present disclosure is to be considered as an exemplification of the principles of the invention and is not intended to
15 limit the invention to the specific embodiments illustrated.

20 The compositions of the present invention are clays that are activated by metal salts that are Lewis acids and are useful for reducing the amount of color impurities in an oil.

25 Throughout this application, the term "oil," and the grammatical variations thereof, includes vegetable-derived, animal-derived as well as marine source-derived fats and fatty oils that are liquids at the particular temperature that is necessary for desired processing of a particular type of oil.

30 In use, the oil and the present oil bleaching composition are combined in a suitable vessel to produce a slurry. The resulting slurry is maintained at an elevated temperature and in vacuo at a pressure no greater than about atmospheric pressure for a time period sufficient to reduce the amount of color impurities of the oil without causing degradation of the oil, i.e., the oil is bleached substantially without

thermal decomposition of the oil. A bleached oil is then recovered from the slurry.

The bleaching is performed at a temperature elevated above room temperature, i.e., at about 5 30 degrees C and higher, but below the temperature that induces thermal decomposition of the oil. A preferred bleaching temperature is in a range of about 50 degrees to about 130 degrees C, more preferably about 60 degrees to about 125 degrees C.

10 The pressure at which the bleaching is performed can be atmospheric or less than atmospheric (subatmospheric), as desired. A suitable reduced pressure is in a range of 1 to about 26 inches of mercury. A preferred reduced pressure is in a range of 15 about 1 to about 5 inches of mercury. A most preferred reduced pressure is about 4 inches of mercury.

The time period sufficient to reduce the amount of color impurities in the oil utilizing the present bleaching compositions usually is in a range of 20 about 5 to about 90 minutes.

Oils that can be bleached using the composition of the present invention include both edible and inedible oils. Illustrative oils are those previously mentioned hereinabove.

25 Materials suitable for the activating treatment of the present invention are clays, preferably having a free moisture content of no more than about 20 weight percent, more preferably no more than about 10 weight percent, i.e., those clay materials characterized 30 by a mineral structure formed by the arrangement of octahedral units and tetrahedral units or by stacked layers formed by an octahedral sheet and one or more tetrahedral sheets of the atoms that constitute the clay mineral structure. Illustrative are the two groups of 35 naturally occurring clay minerals. First is the hornite

group, defined here as including palygorskite and
sepiolite, which have channels formed by octahedral
units and tetrahedral units of the clay mineral
structure. Second is the smectite group including
5 montmorillonites and saponite, which are constituted by
stacked layers formed by an octahedral sheet and one or
more tetrahedral sheets, and mixtures of the foregoing.

Previously acid activated bleaching clays,
such as those commercially available, e.g., FILTROL®
10 105 SF, PURE-FLO® Supreme, and the like, are also
suitable. As to the latter grouping of clay minerals,
the bleaching activity of these acid activated bleaching
clays (usually acid-treated calcium bentonites) can be
further enhanced by the treatment provided by the
15 process of the present invention.

Palygorskite (attapulgitite), a mineral found in
some clays, is a hydrous silicate material represented
by the approximate formula:



See, e.g., Grim, R.E., Clay Mineralogy, 2nd ed.,
McGraw-Hill, Inc., New York, N.Y. (1968), p. 115.

Smectite is a generic term that refers to a
25 variety of related minerals also found in some clays.
The smectite minerals typically occur only as extremely
small particles. Generally, smectite is composed of
units made of two silica tetrahedral sheets with a
central alumina octahedral sheet. Each of the
30 tetrahedra has a tip that points to the center of the
smectite unit. The tetrahedral and octahedral sheets
are combined so that the tips of the tetrahedra of each
silica sheet and one of the hydroxyl layers of the
octahedral sheet form a common layer. See Id., pp. 77-
35 78.

In particular, the smectite family of clays includes the various mineral species montmorillonite, nontronite, hectorite and saponite, all of which can be present in the clay mineral in varying amounts.

5 Other minerals, neither of the smectite genus nor of the hormite variety, that can be present in clay include opal, apatite, calcite, the feldspars, kaolinite, mica, quartz and gypsum, among others.

10 It has been found that addition of certain metal salts to clay, with or without the addition of sulfuric acid, enhances the surface acidity of the clay without a substantial adverse effect on the clay lattice.

15 The amount of available surface acid sites is enhanced by introducing cations of high charge and small radius, such as Al^{+3} , Fe^{+2} , Fe^{+3} , or Ti^{+4} that react with water to make a proton available for further reaction. Metal salts that are Lewis acids are suitable sources of such cations. Optionally, additional protons can be
20 provided by means of a protonic acid treatment using, e.g., sulfuric acid. The combination of both introducing cations of high charge and small radius and providing protons by means of a protonic acid is preferred. Particularly preferred is the addition of
25 $\text{Al}_2(\text{SO}_4)_3$, with relatively small amounts of H_2SO_4 .

The charge and the radius of the ion relates to the ionic potential of an ion. Mason, B., *Principles of Geochemistry 2d*, 155, Wiley and Sons, New York (1958). Ionic potential is the charge of the ion (Z)
30 divided by the radius of the ion (r), and is, in effect, a measure of electronegativity. *Id.*, 155-56. Ionic potentials of several ions are given in Table 1. *Id.*, 156. Cations having ionic potentials in the range of about 2.5 to about 10 are preferred and are provided by
35 the preferred Lewis acid metal salts of the present

invention, i.e., aluminum salts such as aluminum chloride, aluminum sulfate, and the like, iron salts such as ferric sulfate, ferrous sulfate, and the like, as well as titanium salts such as titanium sulfate and the like.

Table 1
Ionic Potentials

Cs ⁺	0.60	Th ⁴⁺	3.9
Rb ⁺	0.68	Ce ⁴⁺	4.3
K ⁺	0.75	Fe ³⁺	4.7
Na ⁺	1.0	Zr ⁴⁺	5.1
Li ⁺	1.5	Be ²⁺	5.7
Ba ⁺	1.5	Al ³⁺	5.9
Sr ²⁺	1.8	Ti ⁴⁺	5.9
Ca ²⁺	2.0	Mn ⁴⁺	6.7
Mn ²⁺	2.5	Nb ⁵⁺	7.5
La ³⁺	2.6	Si ⁴⁺	9.5
Fe ²⁺	2.7	Mo ⁵⁺	9.7
Co ²⁺	2.8	B ³⁺	13
Mg ²⁺	3.0	P ⁵⁺	14
Y ³⁺	3.3	S ⁶⁺	20
Lu ³⁺	3.5	C ⁴⁺	25
Sc ³⁺	3.7	N ⁵⁺	38

For bleaching an oil, the amount of the present bleaching clay that is combined with the oil to be bleached usually is in the range of about 1 to about 5 weight percent, based on the weight of the oil. Lesser or greater amounts can be used, depending upon the oil to be treated and the severity of the desired bleaching treatment.

The acid site enhancement process embodying the present invention can be carried out batchwise, or as a continuous process, as convenient. The mixing of the clay and multivalent metal salts, with or without

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the presence of a protonic acid, during the activation process can be readily achieved by the use of a static mixer, a commercially available blender, or the like expedient. The amount of the multivalent metal ion present is sufficient to enhance the amount of surface acid sites present and usually is in the range of about 0.2 to about 0.5 weight percent for Al and about 0.2 to about 0.6 weight percent for Fe, expressed as weight of the metal and based on the weight of the dry clay.

The present invention is illustrated by the following examples.

EXAMPLE 1: Enhancement of Bleaching by Treatment of Georgia Clays with Lewis Acids or Lewis Acid Metal Salts

Georgia clay, when mixed in the moist state with dry, granular Lewis acids or solutions of Lewis acids, and after an appropriate drying and grinding, produced a bleaching clay exhibiting more bleaching activity than a bleaching clay made by the sulfuric acid treatment alone.

Surface acidity in bleaching clays is controlled by the chemistry and amount of multivalent cations (such as Ti^{4+} , Al^{3+} , Fe^{2+}) exposed or covering the clay surface. By mixing the Georgia clay with 4 to 5 weight percent sulfuric acid, the amount of those extractable metals was doubled.

A highly active also bleaching clay resulted from mixing clay with solutions of $Al_2(SO_4)_3$ and $FeSO_4$ salts at a ratio of the metals of 4:2 by weight. Small amounts of titanium sulfate added to the mixture provided further improvement in bleaching characteristics. The Lewis acid metal salt treated clay of this invention performed better in chlorophyll removal than a sulfuric acid enhanced clay made from the same starting raw material.

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The Lewis acid treated bleaching clay showed better stability than the commercially available bleaching clay (PURE-FLO SUPREME) used for these comparisons. The commercially available bleaching clay used for comparison in this instance was made from a mixture of a high pH (pH value of 7 to 8) clay that is acid activated with 4 to 6 weight percent of sulfuric acid.

Sample preparation

Each raw clay sample was ground to less than 3 mm in largest dimension by a laboratory hammer mill. An aliquot (1500 g) of clay was mixed with various Lewis acid metal salts separately and in combination to yield the optimal activity. Tables 2 and 3 give the ratios and weight percentages of the added metal salts. For comparison, clays were also treated with 4, 5, and 6 weight percent sulfuric acid. After mixing, the samples were dried in an oven to 12 weight percent free moisture (FM). Dried samples were ground to powder by a micropulverizer.

The hydrated salts $\text{Al}_2(\text{SO}_4)_3 \cdot 18 \text{H}_2\text{O}$, $\text{FeSO}_4 \cdot 7 \text{H}_2\text{O}$, and $\text{TiSO}_4 \cdot 8 \text{H}_2\text{O}$ were used. Aluminum sulfate was generally used as a 26.8 weight percent solution. Appropriate amounts of Fe or Ti salts were dissolve in water to produce solutions added at the proportion of 100 ml solution to 1500 g of raw clay. The added amounts are reported as weight percent of the cation based on dry clay (zero weight percent moisture).

Each sample was tested for bleaching activity with canola oil. Canola oil (100 g) containing chlorophyll (26,000 ppb) was combined with the indicated weight percent of clay and bleached at 108 degrees C for 30 minutes under partial vacuum of 26 inches of mercury (0.87 atmosphere). The remaining chlorophyll, red

colors, free fatty acid (FFA) and peroxide values in the bleached oils were measured using standard tests.

The red color of the treated oil was monitored in accordance with American Oil Chemists Society (AOCS) Official Method CC13b-45, and light absorption at 450 nanometers (nm). All clay samples were tested for free moisture and pH. Aluminum and iron concentrations were measured in some selected oil samples. Stability testing on some selected samples was done by running bleaching tests on aged clay.

Table 2 compares the effects on bleaching activity of two treatments: enhancement using Lewis acid metal salts and H_2SO_4 enhancement. The results show that the Lewis acid enhanced product of the present invention has a significantly higher pH, removes chlorophyll better, removes soaps equally well, and has slightly lower FFA compared to the H_2SO_4 enhanced product. Treatment with both 0.312% Al and 1% H_2SO_4 was more effective than treatment with H_2SO_4 but not as effective as treatment with 0.312% Al alone.

The combination of aluminum and iron sulfates gave better chlorophyll removal than either of the individual sulfates alone. Clay treated with aluminum sulfate performed better than clay treated with an equivalent weight percent of aluminum chloride.

Table 2
Enhancement of Bleaching Activity after Various Clay Treatments
(Starting Chlorophyll Concentration 26,000 ppb)

5		% Added	Remaining Chlorophyll (ppb)		pH	Soap Removed	FFA
		(weight % of clay)	Mean	StDev		(ppm)	(%)
10	Al ₂ (SO ₄) ₃	0.078 Al	2441	7.1	5.13	6.09	0.050
		0.234 Al	1752	62.9	4.45	6.10	0.045
		0.312 Al	1663	0.0	4.34	6.08	0.050
		0.390 Al	1720	87.0	4.12	7.61	0.050
		0.468 Al	1730	58.7	5.12	7.61	0.065
		0.540 Al	1727	173.9	4.05	10.65	0.060
15	Al ₂ (SO ₄) ₃ + FeSO ₄	0.312 Al 0.2 Fe	1415	21.1	4.03	7.61	0.050
		0.156 Al 0.4 Fe	1835	83.4	4.05	7.35	0.050
		0.234 Al 0.2 Fe	1666	24.0	4.14		0.060
		0.234 Al 0.4 Fe	1850	173.9	4.02	9.13	
20	FeSO ₄	0.8 Fe	1804	79.9	3.95		
	H ₂ SO ₄	4	2234	97.9	2.84	6.09	0.065
		5	2136	159.8	2.57	7.61	0.065
	AlCl ₃	0.809 Al	2935	107.5	4.00		
		1.012 Al	2412	70.0	4.01		
1.214 Al		2197	59.4	3.83			
25	Al ₂ (SO ₄) ₃ + H ₂ SO ₄	0.312 Al 1 H ₂ SO ₄	1991	72.8	3.16		

**EXAMPLE 2: Effect of Lewis Acid Concentration on
Enhancement of Bleaching**

Further studies examined the effects of adding different concentrations and combinations of Al and Fe. The results are presented in Table 3. One of the more effective treatments was the addition of a combination of salts containing 0.312% Al and 0.4% Fe. The added cation concentration is expressed as based weight percent of dry clay. There was 30-40% less chlorophyll remaining after bleaching with clay subjected to this treatment compared to clay treated with H_2SO_4 . The results of measuring the pH and FFA values were similar to those reported in Example 1. In all tests, Fe remaining in the bleached canola oil was below the detection limit (< 0.1 ppm).

Table 3
Optimization of Clay Treatment

		% Added	Remaining Chlorophyll (ppb)		pH	FFA (%)	FM (%)
		(weight % of clay)	Mean	StDev			
5	$\text{Al}_2(\text{SO}_4)_3$	0.234 Al	2165	83.4	4.11	0.040	9.4
		0.312 Al	1772	13.4	3.92	0.050	9.8
	$\text{Al}_2(\text{SO}_4)_3 + \text{FeSO}_4$	0.234 Al 0.2 Fe	1838	38.2	3.95		5.6
		0.312 Al 0.2 Fe	1765	79.9	3.91		7.6
10		0.390 Al 0.2 Fe	1784	10.6	3.83		9
		0.234 Al 0.4 Fe	1635	40.3	3.87	0.055	7.4
		0.312 Al 0.4 Fe	1502	40.3	3.80	0.060	13.4
		0.390 Al 0.4 Fe	1644	13.4	3.64	0.055	10.8
15	H_2SO_4	4	2240	61.5	2.92	0.065	7.6
		5	2276	52.3	2.66		10.4
		6	2520	77.1	2.47		6.8

EXAMPLE 3: Effect of Lewis Acid Concentration on
Enhancement of Bleaching, Raw Clay Source B

The performance of a different clay treated with combinations of $\text{Al}_2(\text{SO}_4)_3 \cdot 18 \text{H}_2\text{O}$ and $\text{FeSO}_4 \cdot 7 \text{H}_2\text{O}$ was examined. The results, reported below in Table 4, confirm that Lewis acid treatment produces better results than H_2SO_4 treatment, and that 4% $\text{Al}_2(\text{SO}_4)_3 \cdot 18 \text{H}_2\text{O}$ and 2% $\text{FeSO}_4 \cdot 7 \text{H}_2\text{O}$ is the preferred combination of aluminum and iron sulfates to be added. This combination corresponds to an addition of 0.312% Al and 0.4% Fe, the cation concentration being expressed as weight percent of dry clay.

Table 4
Optimization of Al and Fe Addition

		% Added	Remaining Chlorophyll (ppb)		Red Color (Absorption at 450 nm)
		(weight % of clay)	Mean	StDev	
5	$\text{Al}_2(\text{SO}_4)_3 + \text{FeSO}_4$	0.234 Al 0.3 Fe	1580	21	0.9625
		0.234 Al 0.4 Fe	1575	63	0.9765
		0.234 Al 0.5 Fe	1675	24	0.9945
		0.312 Al 0.3 Fe	1668	14	0.9540
10		0.312 Al 0.4 Fe	1489	52	0.9455
		0.312 Al 0.5 Fe	1575	42	0.9655
		0.390 Al 0.3 Fe	1661	143	0.9460
		0.390 Al 0.4 Fe	1562	38	0.9775
		0.390 Al 0.5 Fe	1831	21	1.0475
15	H_2SO_4	4	2169	42	0.8845
		5	2042	188	0.8610
		6	2315	86	0.9145

Table 5 shows the results of additions of Al and Fe cations, in combination with H_2SO_4 , in comparison with the effects of the addition of either of these cations alone. The average of two chlorophyll determinations is presented with the standard deviation (StDev). The additive combination that produced the lowest remaining chlorophyll levels of the Lewis acid metal salts treatments was observed to be that of 0.312% Al and 0.4% Fe together with 2% H_2SO_4 .

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Table 5
Georgia Clay Enhanced with Al, Fe and H₂SO₄

	Al wt.-%	H ₂ SO ₄ wt.-%	Fe wt.-%	Remaining Chlorophyll (ppb)	Remaining Chlorophyll Average ± StDev (ppb)	Red Color	pH
5	0.312	2	0.2	1363 1447	1406 ± 59	6.7 6.7	3.2
	0.312	2	0.4	1299 1225	1262 ± 52	6.5 6.4	3.09
	0.312	1	0.4	1556 1575	1565 ± 14	6.6 6.5	3.46
	0.312	3	0.4	1732 1633	1682.5 ± 70	6.9 6.7	2.83
	-	5	-	1884 1732	1808 ± 107	6.5 6.4	2.82
10	0.312	2	-	1756 1629	1692.5 ± 90	6.9 6.6	3.22
	0.312	-	0.4	1462 1457	1459.5 ± 4	7.3 7.2	4.0
	0.312	1	-	1693 1639	1666 ± 38	7.5 7.4	3.56
	OPT FF			891 837	864 ± 38	5.5 5.5	

15 **EXAMPLE 4: Effect of Lewis Acid Concentration on**
 Enhancement of Bleaching

20 The effect of Ti(SO₄)₂ · 8 H₂O in combination
 with the preceding aluminum and iron sulfate treatments
 was examined. The results are shown in Tables 6, 7 and
 8, below. The presence of Ti⁴⁺, added as
 Ti(SO₄)₂ · 8 H₂O, in addition to aluminum sulfate and
 iron sulfate further enhanced the bleaching performance
 of the treated clays. The slight differences in
 efficiency reflect variability in raw materials and
 25 analytical precision.

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Table 6
Effect of Al, Fe, and Ti Sulfate Treatment
on Bleaching Efficiency of Clay

5		wt.-% Added	Remaining Chlorophyll (ppb)	
			Mean	StDev
	$\text{Al}_2(\text{SO}_4)_3 + \text{FeSO}_4 + \text{TiSO}_4$	0.312 Al 0.4 Fe 0 Ti	2118	190.9
		0.312 Al 0.4 Fe 0.068 Ti	1968	41.7
		0.312 Al 0.4 Fe 0.125 Ti	1897	31.1
10	H_2SO_4	5	2234	55.9

Table 7
Effect of Various Concentrations of Titanium
on Bleaching Efficacy: Study A

15	Sample	wt.-% Added				Remaining Chlorophyll (ppb)	
		H_2SO_4	Al	Fe	Ti	pH	Mean StDev
	1		0.234	0.4	0.063	3.95	1415 17
	2		0.234	0.4	0.125	3.89	1309 7
	3		0.234	0.4	0.188	3.81	1536 13
20	4		0.273	0.4	0.063	3.89	1267 38
	5		0.273	0.4	0.125	3.88	1167 56
	6		0.273	0.4	0.188	3.82	1282 17
	7		0.312	0.4	0.063	3.85	1275 13
	8		0.312	0.4	0.125	3.78	1375 38
25	9		0.312	0.4	0.188	3.76	1804 18
	10	4	-	-	-	3.23	1841 180
	11	5	-	-	-	2.98	1727 1

Table 8
Effect of Various Concentrations of Titanium
on Bleaching Efficacy: Study B

	Sample	wt.-% Added				Remaining Chlorophyll (ppb)	
		H ₂ SO ₄	Al	Fe	Ti	pH	Mean StDev
5	1		0.234	0.4	0.063	3.78	1378 62
	2		0.234	0.4	0.125	3.80	1378 7
	3		0.234	0.4	0.188	3.57	1265 7
	4		0.273	0.4	0.063	3.95	1346 66
10	5		0.273	0.4	0.125	3.82	1464 45
	6		0.273	0.4	0.188	3.58	1550 188
	7		0.312	0.4	0.063	3.92	1385 18
	8		0.312	0.4	0.125	3.66	1380 66
	9		0.312	0.4	0.188	3.55	1329 91
15	10		0.312	0.4	-	4.06	1419 80
	11	5	-	-	-	2.81	1796 8

Table 9
Effect of Clay Source and Lewis Acid
Concentration on Bleaching Efficacy

	Raw Clay Source	wt.-% Added	Remaining Chlorophyll (ppb)	
			Mean	StDev
20	A	0.312 Al 0.4 Fe	1569	34
	B	0.312 Al 0.4 Fe	1335	1
	C	0.312 Al 0.4 Fe	4643	316
	D	0.312 Al 0.4 Fe	1975	24
	E	0.312 Al 0.4 Fe	2237	114
	F	0.312 Al 0.4 Fe	1838	190
25				
30				

**EXAMPLE 5: Effect of Clay Source and Lewis Acid
Concentration on Enhancement of Bleaching**

Clays from several raw material sources were studied as candidates for activation by Lewis acids.

5 The results, shown in Table 9 (above), indicate that the bleaching enhancement achieved varies with the starting clay material.

**EXAMPLE 6: The Effect of Lewis Acid Metal Salts
Treatment on Surface Area and Pore Volume**

10 Treatment with Lewis acid metal salts alters physical characteristics of the clay surface such as clay specific surface area and pore volume.

The changes in clay surface area and pore volume were measured by two techniques: the well-known
15 BET method described in Brunnauer et al., *J. Am. Chem. Soc.* 60: 309 (1938) and the ethylene glycol monoethyl ether (EGME) method. See generally, Bradley, et al., Clays and Clay Min. 10: 117-122 (1961); Brindley, G.W. and Hoffmann, R.W., Clays and Clay Min. 9: 546-556
20 (1960); Carter, et al., Soil Sci. 100: 356-360 (1965).

Table 10 shows the results measured by the BET method for Georgia clay treated with various dosages of sulfuric acid. Surface area, pore volume and the total volume of pores in the range of 20-100 Å all declined
25 with increased acid dosage. In contrast, pore diameter increased with increased acid dosage.

Table 10
Effect of Acid Added to Clay Structure on Pore Size and Pore Volume

	H ₂ SO ₄ %	Surface Area (BET) m ² /g	Total Pore Volume ml/g	Average Pore Diameter, Å	Pore Volume in the range of 20-100 Å, ml/g
5	0	134	0.489	14.6	0.178
	1	135.6	0.497	14.2	0.188
	3	126.3	0.457	14.5	0.173
	5	104.1	0.415	15.9	0.168
10	10	68	0.351	20.7	0.144

The results of measuring surface area by the EGME method for clays treated with various combinations of metal salts are presented in Table 11. The same clay sample was used as the raw material source to simplify comparisons. The average surface area for the metal salt treated clay (500 m²/g) was higher than that of the sulfuric acid treated clay (386 m²/g).

Table 11
Surface Area Measured by EGME

	Metal Added, as Sulfate	Percent Metal Added	SSA m ² /g
20	Al, Fe	0.31, 0.40	511
	Al, Fe	0.23, 0.40	509
	Al, Fe	0.40, 0.20	496
25	Al, Fe	0.27, 0.4	505
	H ₂ SO ₄	5	386

Comparable results using the BET method are provided in Table 12. The changes in the distribution of pore sizes is shown graphically in FIGURE 1. Little change in surface area and average pore diameter was noted with the relatively lower dosages of Al. However, the highest Al dosage produced changes similar to those produced by sulfuric acid treatment.

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Table 12
Surface Area Results, Clay Treated With Various Concentrations in Weight Percent of Al Salt

	SAMPLE	0.078% Al	0.234% Al	0.390% Al	0.540 % Al	4% H ₂ SO ₄
5	BET (m ² /g)	145.5	151.4	145.2	123.5	129.8
	Total Pore Volume (ml/g)	0.4387	0.4423	0.4020	0.3600	0.4104
	Average Pore Diameter (nm)	12.1	11.7	11.1	11.6	12.6
10	Pore Volume (ml/g) In Pore Size Ranges					
	10-20 Å	0.01877	0.01983	0.01452	0.01069	0.01195
	20-30	0.02178	0.02260	0.02116	0.02180	0.01930
	30-40	0.02049	0.02132	0.02359	0.01958	0.01844
	40-50	0.02969	0.01140	0.01367	0.01779	0.02029
15	50-60	0.01881	0.02382	0.01878	0.01678	0.02569
	60-70	0.02229	0.01789	0.02445	0.01978	0.02054
	70-80	0.03718	0.01881	0.01565	0.01510	0.02197
	80-90	0.02742	0.02700	0.01716	0.02521	0.02324
	90-100	0.02858	0.01963	0.01876	0.01831	0.02522
20	100-120	0.04119	0.04116	0.04259	0.03909	0.05152
	120-150	0.04407	0.06281	0.05681	0.04928	0.05150
	150-200	0.05396	0.04043	0.04605	0.03894	0.05000
	200-300	0.00403	0.00824	0.01992	0.01037	0.01191
	> 300	0.00000	0.00000	0.00000	0.00000	0.00000

25

**EXAMPLE 7: Comparison of Physical Characteristics:
Clays Produced on Industrial Scale**

Clays activated by treatment with Lewis acid metal salts were produced using pug mill, rotary dryer, and a Raymond roller mill. The ferrous sulfate heptahydrate was added as a dry powder to the conveyor. Aluminum sulfate solution was sprayed onto the clay in the pug mill. The target moisture was 17% and the grind was 80% -325 mesh. The target addition of the chemical was 0.4 wt.-% Fe and sufficient aluminum sulfate solution to yield 0.312 wt.-% Al. The manual addition of

35

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ferrous sulfate and aluminum sulfate produced some variation during the run.

The samples were tested for bleaching activity with canola oil. The conditions were: 100 g oil
5 containing 26,000 ppb chlorophyll was bleached for 30 minutes under vacuum at 127 degrees C. FIGURE 2 compares the results obtained with the present invention (mean \pm standard error of the mean, N=5) to those obtained with two commercially available bleaching
10 clays, PURE-FLO PRO-ACTIVE (Lot PA 4343EE), and OPTIMUM FF. The adsorption isotherm for the present invention was at or below those for the commercial products.

The physical characteristics of clays activated by treatment with Lewis acids made in this
15 Example are compared to the two commercially available clays in Table 13. The Lewis acid enhanced product shows a 20% improvement in chlorophyll removal compared with H₂SO₄ enhanced material from the same homogeneous stockpile.

20 Variations in measured parameters probably resulted from inconsistent manual addition of the Lewis acids in this case. Variations were especially noticeable at low product dosages.

Pore volume measurements are presented in
25 Table 13. The fraction of pores in the 20 - 100 Å size range, believed to have greatest effect on chlorophyll removal, are highest in the metal salt enhanced material. In this critical pore size range, the Lewis acid enhanced clay had 15% more pore volume than the
30 H₂SO₄ enhanced clay.

Filtration rates measured using the Lewis acid activated clay of the present invention were similar to those of the commercially available bleaching clay, PURE-FLO SUPREME.

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Table 13
Comparison of Physical Characteristics

		FM	FFA	PV	Surface Area	Total Pore Volume	Average Pore Diameter	Pore Volume 20-100 Å
	Clay	pH	(%)	(%)	(meq/kg)	(m ² /g)	(nm)	(ml/g)
5	Al + Fe Treated (Mean, N = 5)	3.96	13.7	0.05	2.96	137.8	0.313	9.07
	Pure-Flo Supreme Pro-Active ¹	3.07	14.4	0.055	2.9	141.2	0.299	8.49
10	Optimum FF ²	3.22	8.6	0.055	3.0	214	0.3	5.61

¹ H₂SO₄ - enhanced bleaching clay

² Bleaching clay commercially available from Süd Chemie.

Product Stability

No changes in activity have been detected during the first two weeks. FIGURE 3 shows the averaged bleaching results of five selected samples, collected during the same production run. The chlorophyll removal results for the clay activated by Lewis acid metal salts are better than those of acid activated clays initially. The clay activated by Lewis acid metal salts retains its superior bleaching properties for the duration test.

This invention has been described in terms of specific embodiments set forth in detail. It should be understood, however, that these embodiments are presented by way of illustration only, and that the invention is not necessarily limited thereto. Modifications and variations within the spirit and scope of the claims that follow will be readily apparent from this disclosure, as those skilled in the art will appreciate.

WE CLAIM:

1. A method for producing a bleaching clay which comprises combining a clay mineral with a metal salt that is a Lewis acid in an amount sufficient to enhance surface acid sites present in the clay mineral.
2. The method in accordance with claim 1 comprising the additional step of drying the bleaching clay to a free moisture content of no more than about 35 weight percent.
3. The method in accordance with claim 1 wherein said Lewis acid provides cations having an ionic potential greater than 2.5.
4. The method in accordance with claim 1 wherein said Lewis acid is aluminum sulfate.
5. The method in accordance with claim 1 wherein said Lewis acid is ferric sulfate.
6. The method in accordance with claim 1 wherein said Lewis acid is ferrous sulfate.
7. The method in accordance with claim 1 wherein said Lewis acid is titanium sulfate.
8. The method in accordance with claim 1 wherein said Lewis acid is aluminum chloride.
9. A bleaching clay produced in accordance with the method of claim 1.
10. The method in accordance with claim 1 wherein the clay is an attapulgite-smectite mixture.
11. The method in accordance with claim 1 wherein the clay is a smectite-opal mixture.
12. The method of claim 2 wherein the bleaching clay is dried to a free moisture content of no more than about 20 weight percent.
13. The method of claim 2 wherein the bleaching clay is dried to a free moisture content of no more than about 10 weight percent.

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14. A method for producing a bleaching clay which comprises combining a clay mineral with a mixture of metal salts that are Lewis acids present in an amount sufficient to enhance surface acid sites present in the clay mineral.

15. The method in accordance with claim 14 wherein said Lewis acids provide cations having an ionic potential greater than 2.5.

16. The method in accordance with claim 14 wherein said mixture includes aluminum sulfate and ferric sulfate.

17. The method in accordance with claim 14 wherein said mixture includes aluminum sulfate, ferrous sulfate and titanium sulfate.

18. The method in accordance with claim 14 wherein said mixture includes aluminum sulfate and ferrous sulfate.

19. The method in accordance with claim 14 wherein said mixture includes aluminum sulfate, ferrous sulfate and titanium sulfate, as well as sulfuric acid.

20. A bleaching clay produced in accordance with the method of claim 14.

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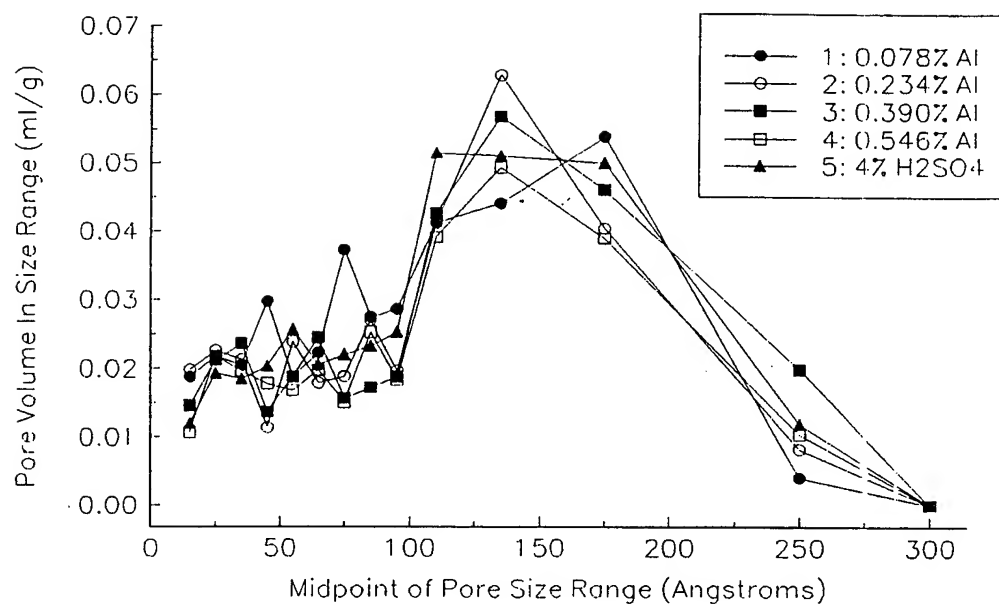


FIGURE 1

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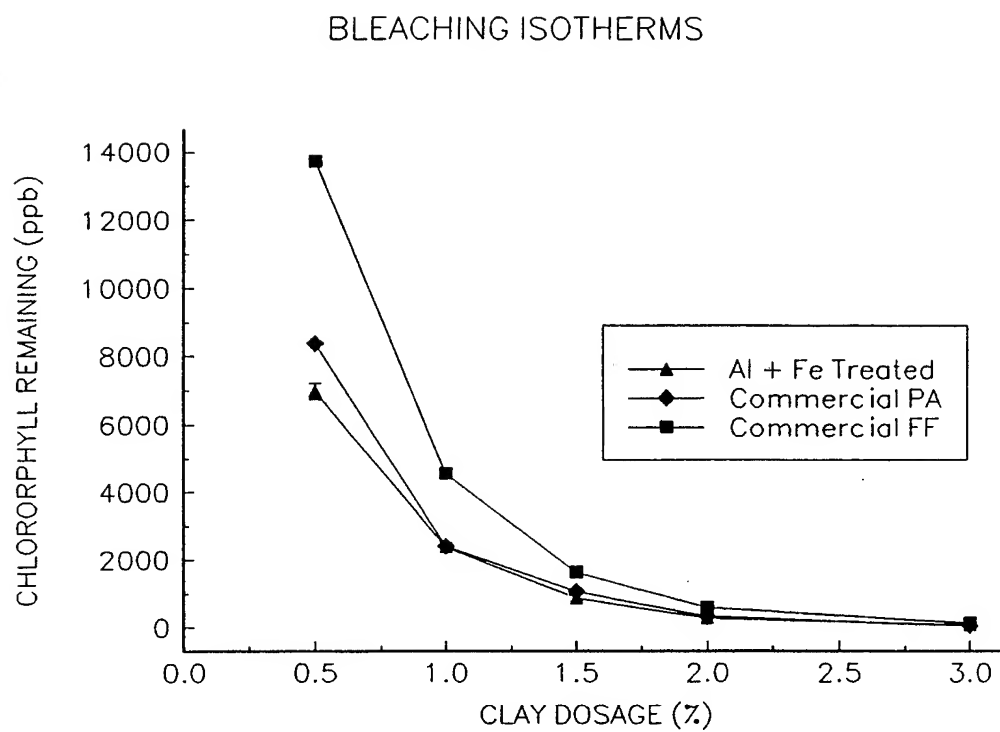


FIGURE 2

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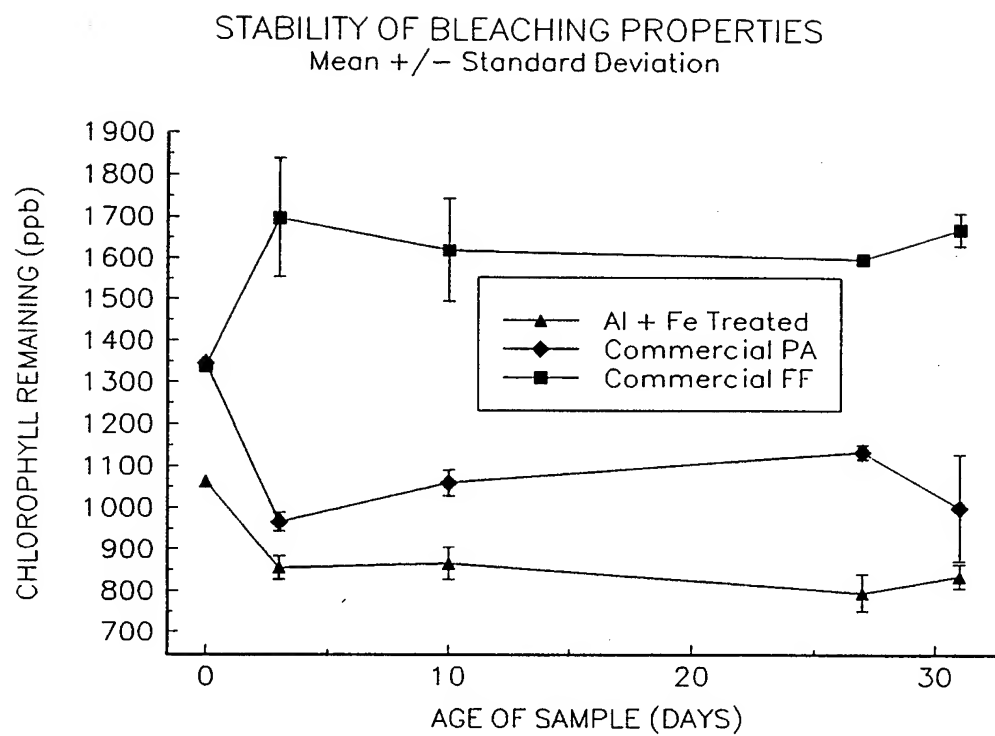


FIGURE 3

INTERNATIONAL SEARCH REPORT

International application No.
PCT/US96/11081

A. CLASSIFICATION OF SUBJECT MATTER

IPC(6) : C09K 3/32; C04B 33/13

US CL : 106/287.17; 501/146; 502/63, 73, 74, 80

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 106/287.17; 501/146; 502/63, 73, 74, 80

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

NONE

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

NONE

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 5,248,641 A [BAUER ET AL] 28 SEPTEMBER 1993 (28.09.93), col. 3, lines 48-50, col. 4, lines 1-5.	1-5, 9, 12-16, 20
X	DE DD270 058 A1 [HOFFMAN ET AL] 19 JULY 1989 (19.07.89), claims 1-4.	8
A	US4,128,263 A [TRAXLER ET AL] 05 DECEMBER 1978 (05.12.78), see abstract.	1-20

☐ Further documents are listed in the continuation of Box C. ☐ See patent family annex.

* Special categories of cited documents:	*T	later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
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P document published prior to the international filing date but later than the priority date claimed		

Date of the actual completion of the international search

01 AUGUST 1996

Date of mailing of the international search report

02 DEC 1996

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